

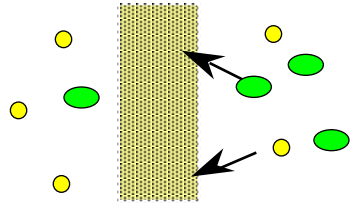
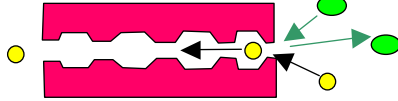
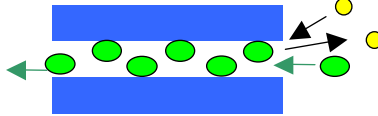
# Next Generation Membrane Materials and Structures for Energy-Efficient Gas Separations

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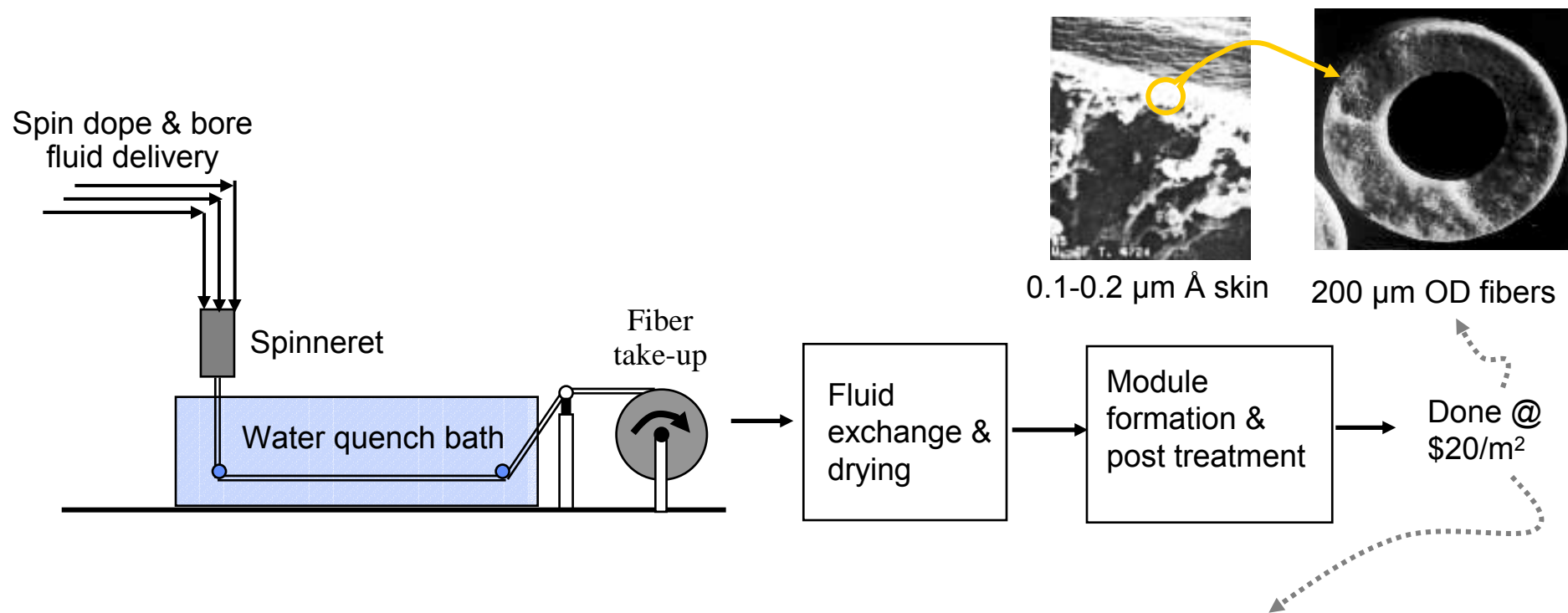
- Revolutionary **vs.** evolutionary advancement strategies
- Hybrid materials— the key evolutionary step
- Fundamental hurdles to making this evolutionary step
- Conclusions & projections

# Sorption-diffusion membranes dominate large scale applications

Sorption-Diffusion Permselectivity, 
$$\alpha_{AB} = \frac{[P_A]}{[P_B]} = \frac{[S_A]}{[S_B]} \frac{[D_A]}{[D_B]}$$

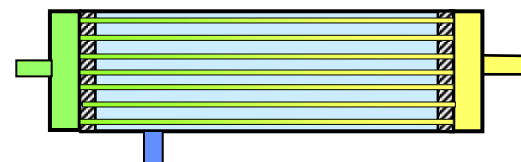
Type	Key Sorption-Diffusion Membrane Types	
<b>A. Polymeric</b> solution- diffusion		<p>Flexible polymers enable selective permeation of the smallest <b>and/or</b> the most condensable (soluble) penetrant</p> <p>--- but encounter limits in <math>\alpha_{AB}</math> vs <math>P_A</math></p>
<b>B. Molecular</b> sieving ( <b>small</b> <b>pore</b> zeolites, & carbons)		<p>Rigid morphology enables highly size selective diffusion jumps favoring <b><u>smallest size</u></b> penetrant</p> <p>--- but large modules are expensive &amp; hard to make.</p>
<b>C. Surface</b> diffusion ( <b>large</b> <b>pore</b> zeolites, glasses, carbons)		<p>Rigid morphology enables <b><u>most condensable</u></b> penetrant to exclude less condensable (often smaller) penetrant</p> <p>---again, large modules are expensive &amp; hard to make.</p>

State-of-the-art hollow fiber spinning processes (50-100 meters/min) allow multiple parallel lines for high throughput, low membrane costs

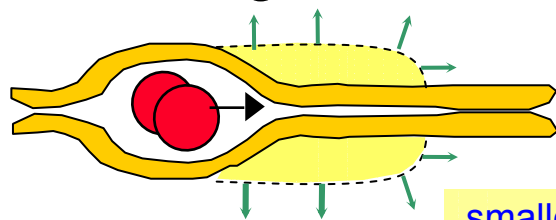


For a large membrane area applications, current membranes (without pretreatment costs) can cost 50% less than competitive technologies— but pretreatment needs sometimes greatly reduce this advantage— **more robust, but still economical** membranes are needed!

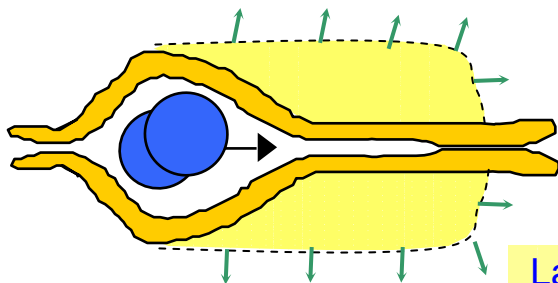
>10<sup>6</sup> fibers, 200 μm OD fiber with 0.1-0.2 μm Å skin in module is currently possible



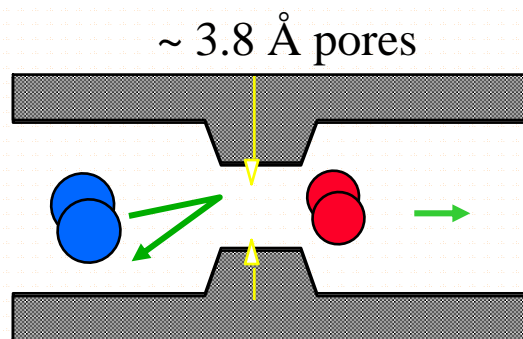
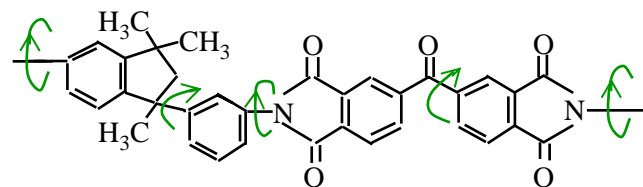
If the “zone of activation” polymers cannot be controlled with ever-increasing for accuracy—can selectivity still be increased?



smaller zone of  
activation for  $O_2$

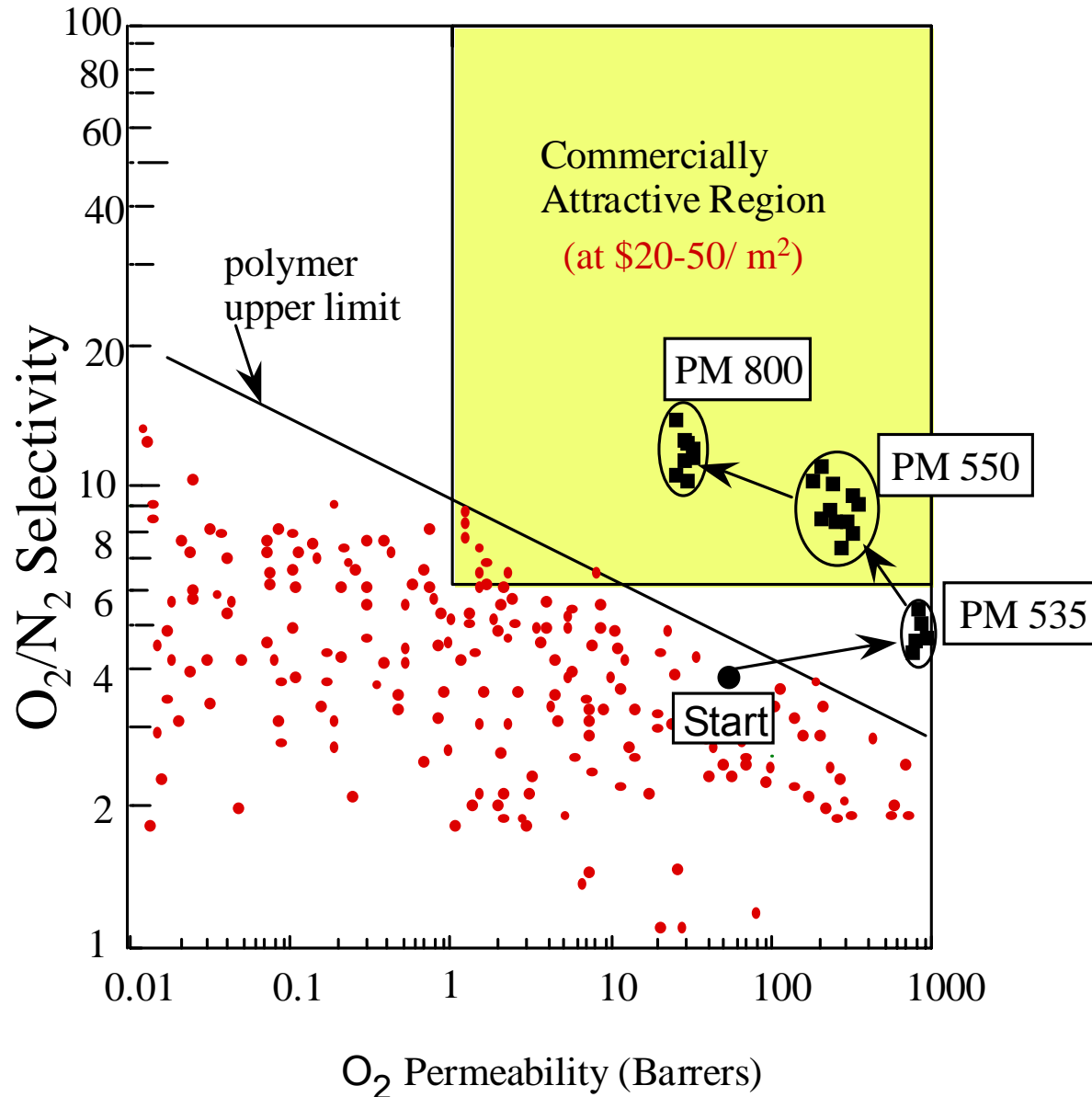


Larger zone of  
activation for  $N_2$



Since thermal & chem. stability & selectivity  $\uparrow$  for mol. sieve carbons and/or inorganics, do they offer **actual** solutions for large scale applications?

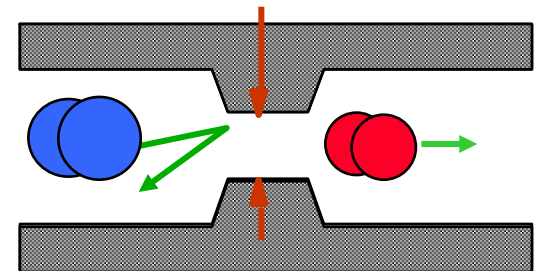
# Tailored carbons & inorganic membranes offer a “technical” solution for many gas & vapor applications



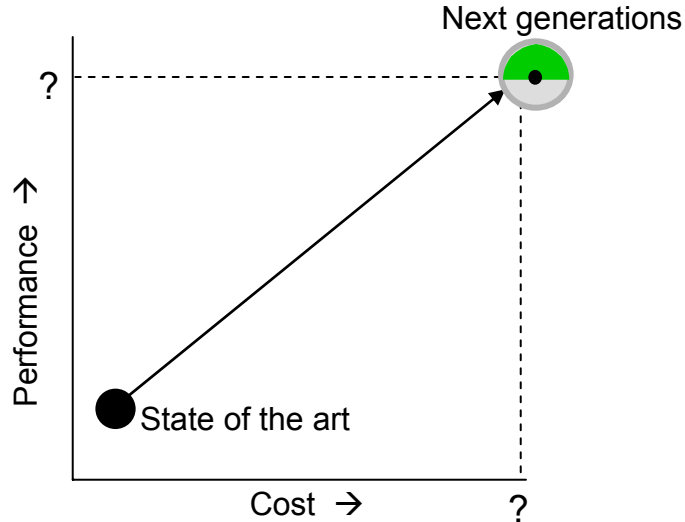
2-4 orders of magnitude faster processing for polymeric allows much lower \$/m<sup>2</sup> vs. carbons & inorganics.

Additional innovative research is needed to provide carbons & inorganics a place in large scale applications.

controllable pore sizes  $\pm 0.1$  Å



# Moving to the Next Generation Involves Performance & Cost Issues



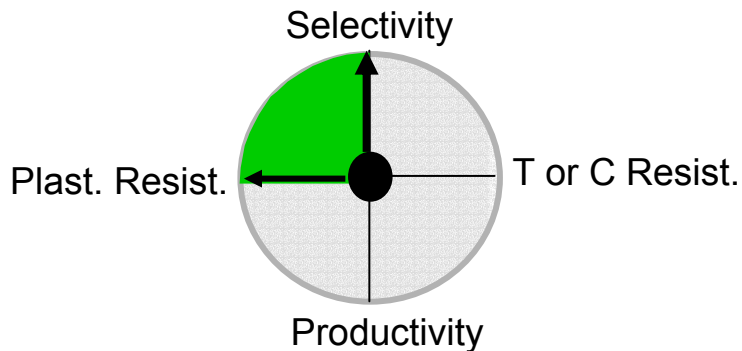
**“Performance Increase” can mean different things:**

I : Increased selectivity

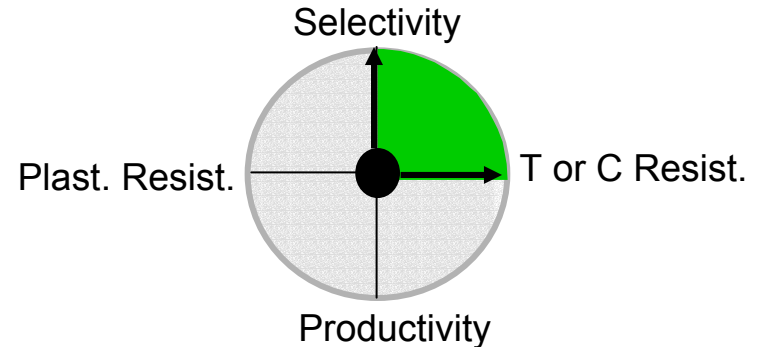
II : Increased productivity (useful but less critical need)

III : Increased plasticization resistance--maintain selectivity

IV : Increased thermal (T) or chemical (C) resistance



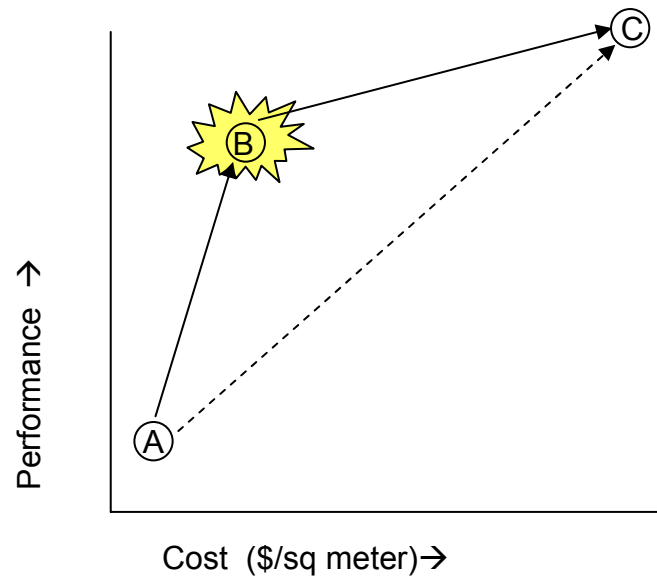
**Vs.**



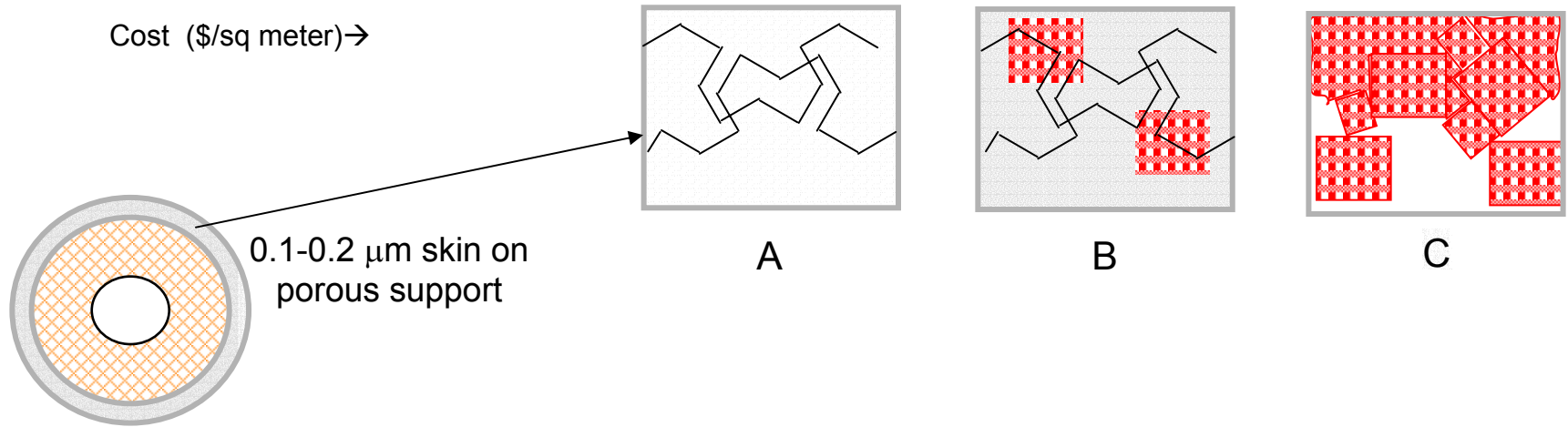
Intrinsically more selective & more swelling resistant— more broadly applicable

Intrinsically more selective & more thermally or chemically resistant—useful, specialty applications

# Revolutionary ( $A \rightarrow C$ ) vs. Evolutionary ( $A \rightarrow B \rightarrow C$ ) Strategies

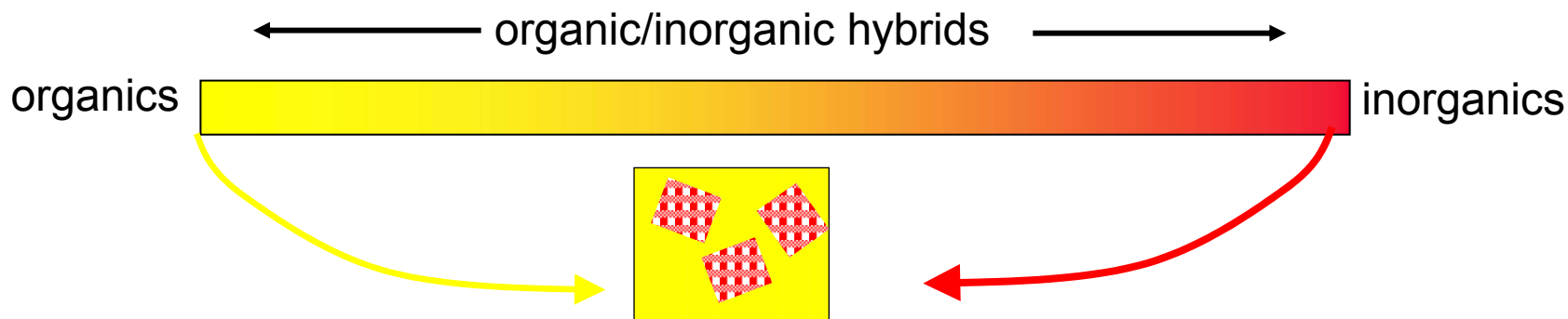


A: current organic polymers  
B: mixed matrix hybrids  
C: pure inorganics or carbons

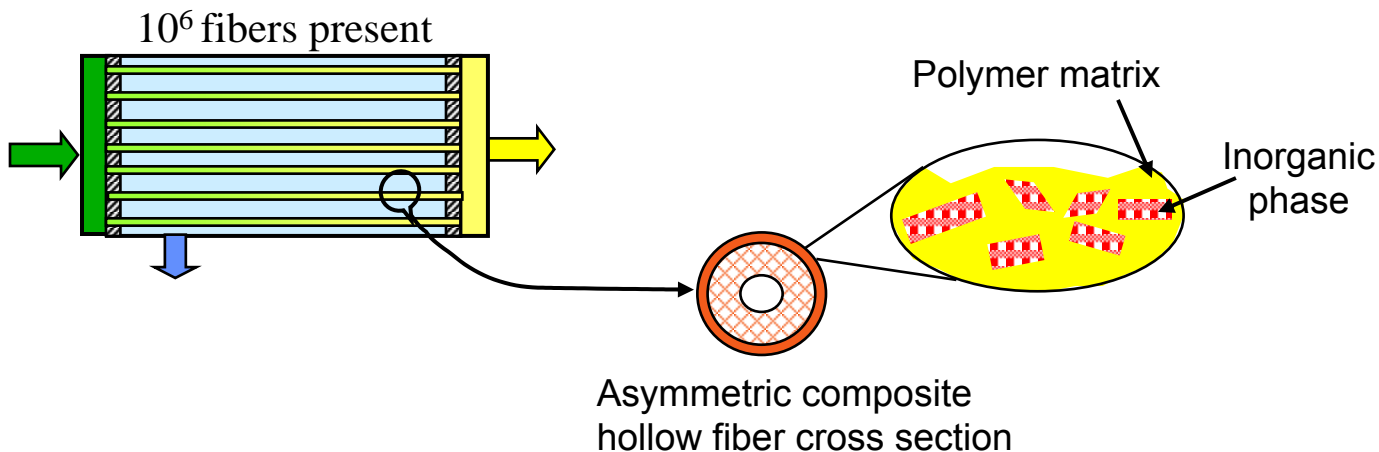
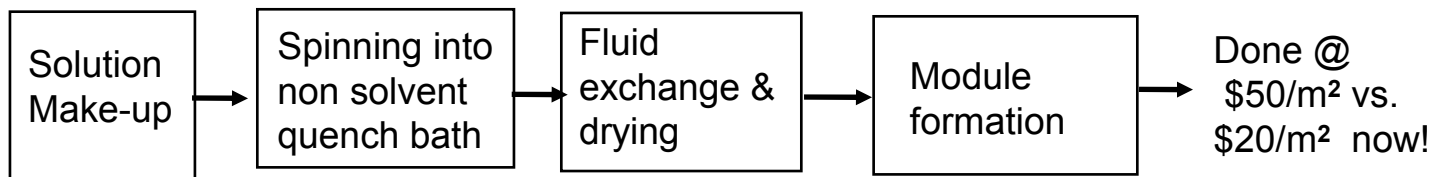


Asymmetric hollow  
fiber cross section—  
current state of the art

# Organic-Inorganic Hybrids May Maintain Low Costs of Current Organic Polymers & Approach Performance of Inorganics



Integrate into current membrane manufacturing process (100 m/min)

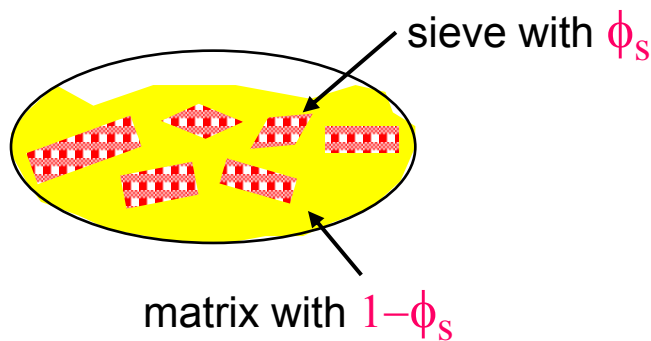




# How to Achieve Practical Mixed Matrix Membranes? - - the first step involves sieve & polymer material “matching”

## A fundamental framework exists to guide “materials selection” ----

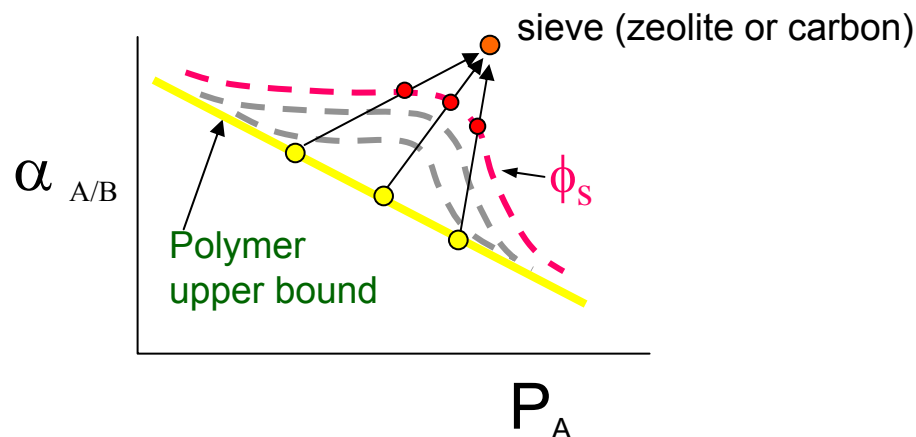
For a selected sieve & volume fraction ( $\phi_s$ ), composite models predict “Enhancement Regions” above polymer upper bound line. (Sieve permeability can be “calibrated” using a reference polymer & then matched to appropriate upper bound polymer matrix)



e.g. Maxwell model for component **A** or **B**

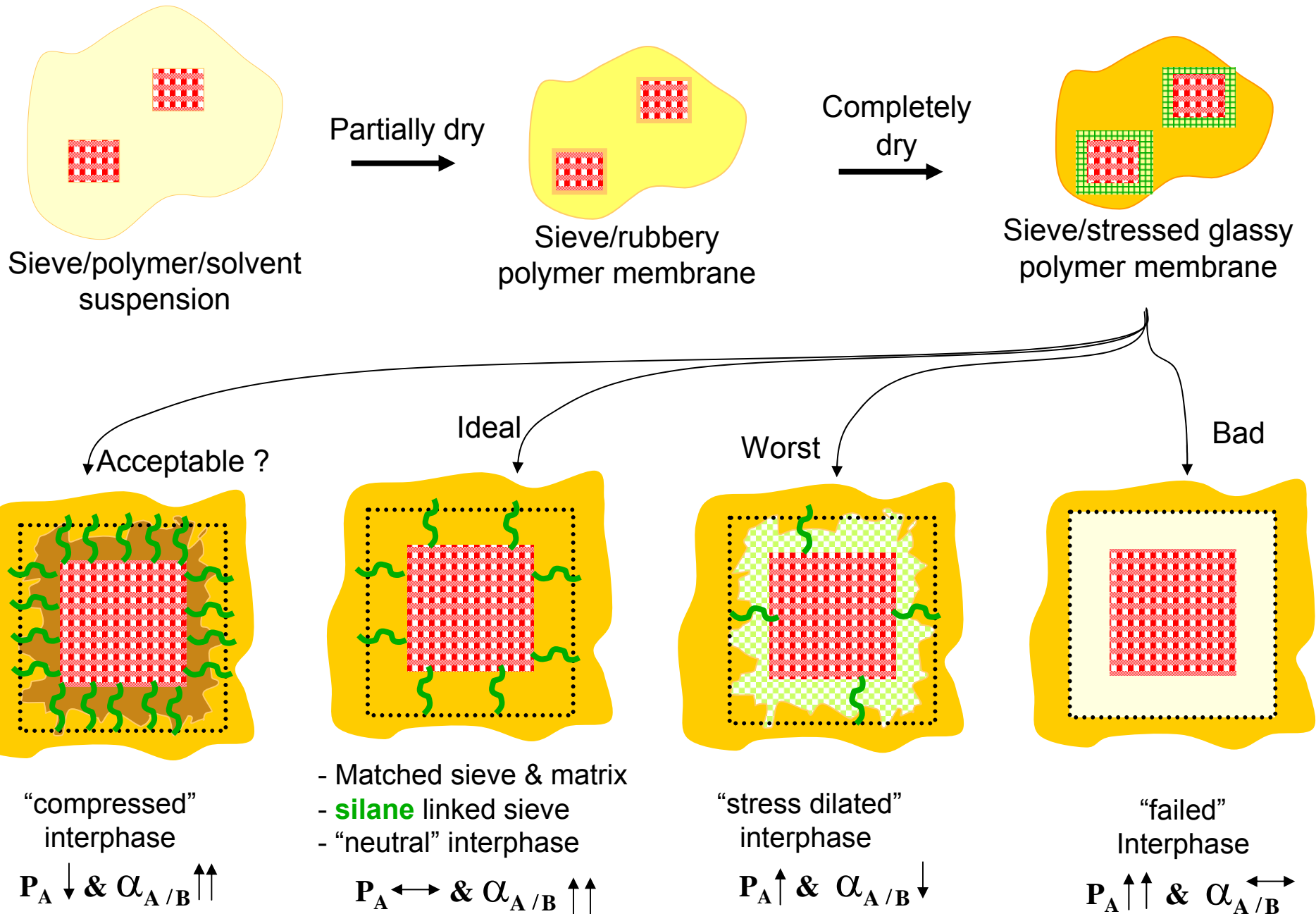
$$P_c = P_m \left[ \frac{P_s + 2P_m - 2\Phi_s (P_m - P_s)}{P_s + 2P_m + \Phi_s (P_m - P_s)} \right]$$

$$\alpha_{A/B} = P_{cA}/P_{cB} \text{ from above model}$$



... But the world includes nonideal realities that must be controlled !

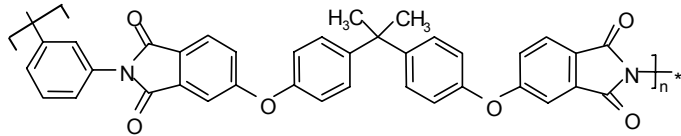
# Non-Ideal Effects: Shrinkage/Coupling/Compatibility Issues



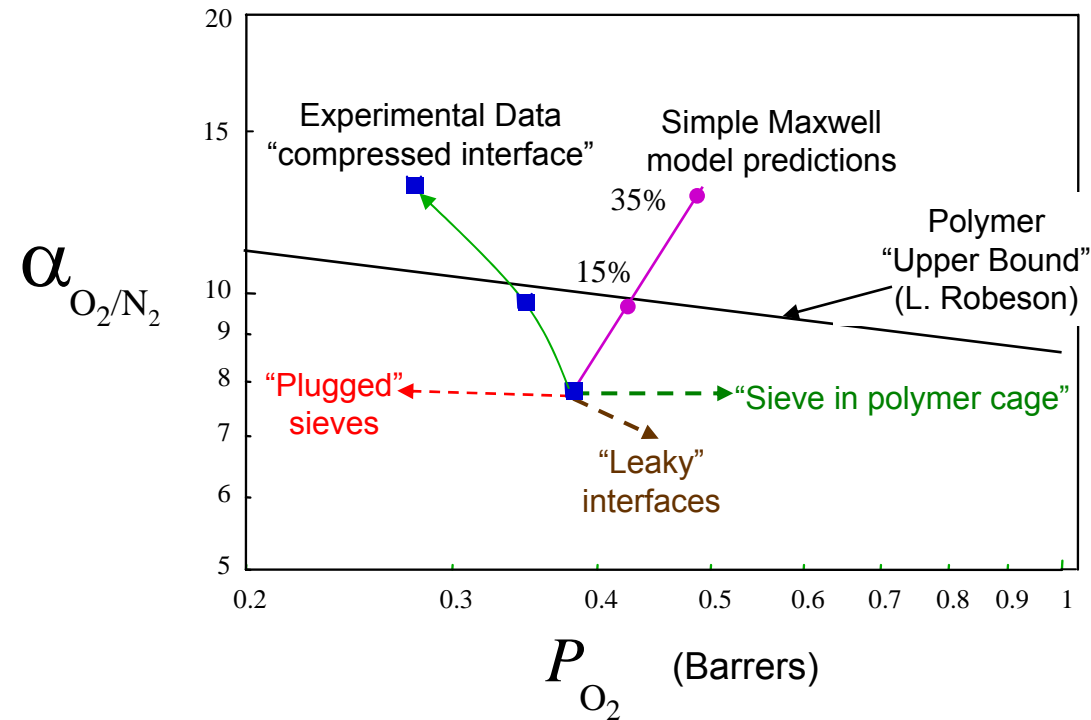
# Ultem®-4A Zeolite Mixed Matrix Materials

Ultem® 1000 polyetherimide (GE)

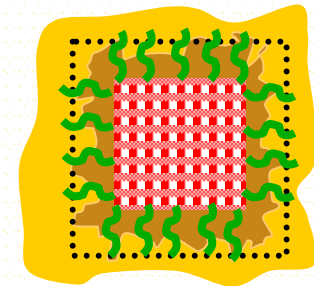
$T_g \sim 220^\circ \text{C}$



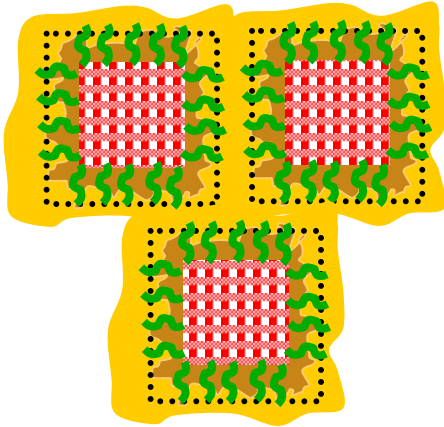
Zeolite 4A  
Molecular Sieve



Performance above upper bound  
 $\alpha_{\text{O}_2/\text{N}_2} > 13$  for pure & mixed gas feeds show expected selectivity but lower permeability--- suggesting a “compressed interface”

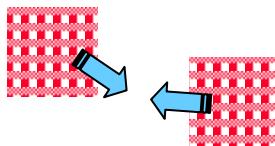
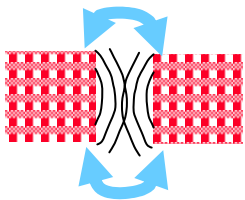


# Key fundamental questions impact materials & spinning topics



- How are sub-nanometer level properties of flexible chain organic polymers affected near surfaces of rigid submicron solids?
  - transport properties in the *nanometer* domain near solid surfaces *versus* the bulk polymer “far” from the surface?
  - effective mechanical properties (modulus & transport properties) as “zones of influence of dispersed solids overlap in casting dopes & vitrified hybrid material ?

Van der Waals attractions



Collision-induced aggregations

- How do millisecond time-scale events during formation of asymmetric skinned structures affect properties noted above compared to the case of a “simple” solution cast dense film?

# Conclusions, projections... and next steps needed:

- Hybrid materials can expand membrane-based gas separation applications
- Morphologies at multiple structural levels and the impact of processing approaches on these morphologies must be understood better
- Control of nanoscale interfaces between the domains in hybrid materials is the *key hurdle* to inhibiting the transition from lab-scale to a production scale
- Better ways to probe adhesion and the resulting influence on the transport properties of the interphase region between the two phases is needed
- Key questions involved in this technology push the state of the art of theory
- & characterization techniques in the materials science & engineering fields
- Involvement of diverse “non-membrane” materials science & engineering
- experts is badly needed in this field